

Research



Cite this article: Hinton EM, Hogg AJ, Huppert HE. 2020 Shallow free-surface Stokes flow around a corner. *Phil. Trans. R. Soc. A* **378**: 20190515.
<http://dx.doi.org/10.1098/rsta.2019.0515>

Accepted: 31 March 2020

One contribution of 14 to a theme issue ‘Stokes at 200 (Part 1)’.

Subject Areas:

volcanology, mathematical modelling, applied mathematics

Keywords:

viscous flows, gravity currents, lava flows

Author for correspondence:

Edward Hinton
e-mail: eh546@cam.ac.uk

Shallow free-surface Stokes flow around a corner

Edward M. Hinton¹, Andrew J. Hogg² and
Herbert E. Huppert³

¹Bullard Laboratories, University of Cambridge, Cambridge CB3 0EZ, UK

²School of Mathematics, University of Bristol, Bristol BS8 1UG, UK

³Institute of Theoretical Geophysics, King's College, University of Cambridge, Cambridge CB2 1ST, UK

EMH, 0000-0002-2204-1204

The steady lateral spreading of a free-surface viscous flow down an inclined plane around a vertex from which the channel width increases linearly with downstream distance is investigated analytically, numerically and experimentally. From the vertex the channel wall opens by an angle α to the downslope direction and the viscous fluid spreads laterally along it before detaching. The motion is modelled using lubrication theory and the distance at which the flow detaches is computed as a function of α using analytical and numerical methods. Far downslope after detachment, it is shown that the motion is accurately modelled in terms of a similarity solution. Moreover, the detachment point is well approximated by a simple expression for a broad range of opening angles. The results are corroborated through a series of laboratory experiments and the implication for the design of barriers to divert lava flows are discussed.

This article is part of the theme issue ‘Stokes at 200 (Part 1)’.

1. Introduction

Viscous gravity currents are abundant in nature and industry and their modelling began with Sir George Stokes' equations for creeping flow. His ideas in this area have been applied to gravitationally driven viscous flows in diverse fields including glass manufacture, lava flows, coating and printing processes, food manufacture and many biological settings [1]. These flows often encounter fixed obstructions, for example in thin film flow around nuts within aeroengine chambers or when a

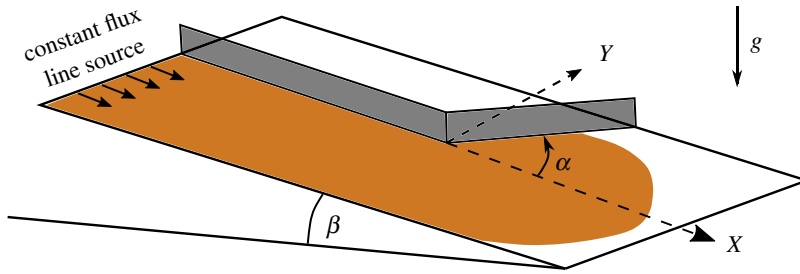


Figure 1. Schematic for gravitationally driven viscous flow down an inclined plane at an angle β to the horizontal. The channel expands with opening angle α to the downslope direction, which we take to be the X axis, while the Y axis is in the cross-slope direction. (Online version in colour.)

lava flow interacts with a barrier [2,3]. Detailed knowledge of the deformation of the free surface is essential for understanding and informing engineering decisions and design.

The interaction between gravity-driven flows and topographic mounds has been well studied and controls on when the mound is surmounted by the flow have been determined [4–9]. There have also been theoretical, numerical and experimental analyses of the flow behaviour upstream of surface piercing cylinders of various cross-sections [2,10–12]. These works have shown that there may be a dry zone (in which there is no fluid) downstream of the obstruction and there have been investigations into the location and extent of the dry zone in the regime that capillary forces play a dominant role [11]. However, at larger length scales, for which the effects of surface tension are negligible, the dependence of the dry zone shape on the obstruction cross-section is not yet well understood.

The present work addresses aspects of this problem and our results have important implications for the optimal design of lava flow barriers. While the previous upstream analyses provide valuable estimates of the barrier height that is required to prevent overtopping by the oncoming flow, it is also important to quantify the controls on the downstream dry zone. The downstream behaviour is challenging to model because of the complex interaction between the spreading fluid and the back of the obstruction, which may lead to the fluid detaching from the barrier to leave a ‘dry’ (fluid-free) zone. To make progress in studying the downstream interaction, we consider the more straightforward geometry of a semi-infinite channel whose wall opens at a vertex downstream (figure 1). The flow detaches from the angled wall at some distance downstream and a major aim of this work is to quantify how the detachment distance along the wall, d , depends on the wall opening angle, α and the depth of the oncoming flow. It is noteworthy that the viscously dominated dynamics analysed in this study are very different from situations in which the flow has significant inertia and detaches at the vertex.

Since a constant flux of fluid is supplied from upstream, the only length scale in the problem is the oncoming flow depth, H_∞ . This enables the derivation of a parameter-free governing equation in §2, using a lubrication approximation. We introduce the numerical method in §3 and present contour plots of the steady flow depth. The dimensionless wall detachment location depends only on the opening angle, α . We show that the contact line where the flow depth vanishes is relatively insensitive to the opening angle and is well described by a simple similarity solution, with a single virtual origin for any opening angle. The results demonstrate that away from the vertex, the influence of the wall and the downslope component of gravitational slumping are negligible and the flow is governed by a balance between the component of gravity acting down the slope and the cross-slope slumping (§§4 and 6). In addition, we construct an exact solution for the special case of $\alpha = \pi$, which corresponds to the abrupt end of the channel wall at $x = y = 0$ (§5). This solution is used to validate the numerical results and to demonstrate the utility of the similarity solution. New experimental results are presented in §7 and these show good agreement with our theoretical and numerical predictions for the detachment distance. We conclude with a

brief discussion of the implications of our results in the context of lava flow barrier design and infer that the design of the downstream side of barriers has little influence on the extent of the fluid-free zone that is safely protected.

2. Formulation

We consider flow down a channel inclined at an angle β to the horizontal (figure 1) and focus on the steady state that develops at long times after transient effects associated with the passage of the front have decayed. The channel opens at the origin in (X, Y) coordinates so that the shape of its wall is given by $Y=0$ for $X < 0$ and $Y=X \tan \alpha$ for $X > 0$ (figure 1). Fluid is supplied with constant flux, Q per unit width, from a line source far upstream, which is semi-infinite in Y ($-\infty < Y < 0$). The flow thickness far upstream is a constant that may be obtained by balancing the downslope component of gravity with the viscous stresses [13,14]

$$H_{\infty} = \left(\frac{3\mu Q}{\rho g \sin \beta} \right)^{1/3}, \quad (2.1)$$

where μ , ρ and g are the dynamic viscosity, the density of the fluid and gravitational acceleration, respectively. We use the lubrication approximation to determine the hydrostatic pressure and velocities in the fluid [15]. Local mass conservation is applied to the velocities to obtain [14]

$$\frac{\partial H}{\partial T} = \frac{\rho g \sin \beta}{3\mu} \left[\cot \beta \frac{\partial}{\partial X} \left(H^3 \frac{\partial H}{\partial X} \right) + \cot \beta \frac{\partial}{\partial Y} \left(H^3 \frac{\partial H}{\partial Y} \right) - \frac{\partial H^3}{\partial X} \right]. \quad (2.2)$$

In this expression we have assumed that the effects of surface tension are negligible; for the experiments described below the capillary length is approximately 2 mm [12], which is much smaller than the streamwise length scale. On adopting dimensionless variables $h = H/H_{\infty}$ and $(x, y) = [X/(H_{\infty} \cot \beta), Y/(H_{\infty} \cot \beta)]$, we find that the steady governing dimensionless equation is

$$\frac{\partial h^3}{\partial x} = \nabla \cdot (h^3 \nabla h), \quad (2.3)$$

while the dimensionless flux in the x and y directions is

$$\mathbf{q} = h^3 \left(1 - \frac{\partial h}{\partial x}, -\frac{\partial h}{\partial y} \right). \quad (2.4)$$

We next describe the boundary conditions for the steady flow. The line source is far upstream of the wall vertex and the line source is semi-infinite. Thus $h \rightarrow 1$ as $x \rightarrow -\infty$ and $h \rightarrow 1$ as $y \rightarrow -\infty$. There is no-flux, $\mathbf{q} \cdot \mathbf{n} = 0$, into the angled wall, where the normal direction to the angled wall is $\mathbf{n} = (\sin \alpha, -\cos \alpha)$. Thus the boundary condition on $y = x \tan \alpha$, $x > 0$, may be written as

$$\left(1 - \frac{\partial h}{\partial x} \right) \tan \alpha + \frac{\partial h}{\partial y} = 0 \quad \text{provided that } h > 0. \quad (2.5)$$

Downstream of the point where the flow detaches from the wall, there is a contact line, $y = y_c(x)$, where the current depth first vanishes: $h(x, y_c(x)) = 0$. We denote the dimensionless distance along the wall at which the flow detaches by d . This nondimensionalized distance depends only on the opening angle α and we write $d = f(\alpha)$. One of the main aims of this work is to determine this dependence. We note that f is a decreasing function of α and $f(\alpha) \rightarrow \infty$ as $\alpha \rightarrow 0$ because the flow does not detach in this limit.

Our model neglects the no-slip boundary condition at the channel wall in accordance with the leading order lubrication model. We have also neglected surface tension, which may become very significant near the contact line (see, for example, [16]). A detailed local treatment of these effects would be needed to complete the solution but they do not affect bulk behaviour and hence can be neglected for our purposes. For a detailed study of the flow near the wall associated with no-slip and matching with the bulk flow, see [17].

3. Numerical method

We use a finite-element method to integrate the steady governing equation (2.3) numerically. The routine is part of Matlab's Partial Differential Equation ToolboxTM, which uses adaptive mesh generation. The steady state is found iteratively; we take an initial guess to be $h = 1$ everywhere and iterate until a converged solution is found. A similar approach has previously been used for flow over a mound and flow past a cylinder [9,12]. We solve the system with the following boundary conditions. There is no normal flux ($\mathbf{q} \cdot \mathbf{n} = 0$) into the wall along $y = 0$ for $x < 0$ and $y = x \tan \alpha$ for $x > 0$. There is also no flux across the domain boundary at $y = -c$. Constant flux ($\mathbf{q} \cdot \mathbf{n} = 1$) is supplied at the upstream boundary, $x = -a$, $-c < y < 0$. Finally, we apply a free-flux condition ($\partial h / \partial x = 0$) at the downstream boundary at $x = b$, $-c < y < b \tan \alpha$. The domain size is determined by the parameters a , b and c . The system is solved with an initial choice of a , b and c and then they are increased and the system solved again. This process is repeated until increasing the domain size further has a negligible influence on the solution. In the case $\alpha = \pi/4$, for example, the domain size is given by $a = 5$, $b = 20$ and $c = 15$. Note that the contour plots presented in this paper include only the region of interest rather than the entire domain of the numerical method. Typically, the mesh for the finite-element method contains approximately 100 000 triangles, which provides sufficient resolution. Contour plots of the steady flow thickness are shown in figure 2 for two values of the angle, α .

The nonlinear diffusive terms on the right-hand side of (2.3) become negligible when h is very small. The original numerical scheme was not effective in this regime. It was necessary to add a small flux out of the open wall to coat the region in which $h = 0$ with a thin film. The modified boundary condition along $y = x \tan \alpha$ is $\mathbf{q} \cdot \mathbf{n} = \epsilon$ where the parameter ϵ was selected to be as small as possible while enabling the code to run efficiently and typical values were 10^{-7} . The influence of ϵ is predominantly seen at the steep edges of the current, which are slightly smoothed (for example, see figure 3*a*). Beyond the steep edge of the current, where we anticipate that the flow depth vanishes, the calculated flow depth is at most $h = 10^{-2}$. We use this value (rather than $h = 0$) to define the edge of the current and obtain the detachment point and the location of the contact line [$y = y_c(x)$].

4. Far-field similarity solution ($x \gg 1$)

Sufficiently far downslope from the wall detachment point, ($x \gg 1$), the governing equation (2.3) may be approximated by [9,14,18]

$$\frac{\partial h^3}{\partial x} = \frac{\partial}{\partial y} \left(h^3 \frac{\partial h}{\partial y} \right) \quad (4.1)$$

and the downstream flow is unlikely to be effected by the details near the vertex. The upstream boundary condition at $x = 0$ is given by $h = 1$ in $y < 0$ and $h = 0$ in $y > 0$. Also $h \rightarrow 1$ as $y \rightarrow -\infty$ because the upstream line source is semi-infinite. The system is self-similar with scaling $y \sim x^{1/2}$ and the omitted streamwise diffusive term, $\partial(h^3 \partial h / \partial x) / \partial x$, relative to the advective term $\partial h^3 / \partial x$ is therefore of order $1/x$ and negligible in the far-field ($x \gg 1$). We transform equation (4.1) using the similarity variables, $\eta = y/x^{1/2}$ and $h(x, y) = \chi(\eta)$, to

$$-\frac{1}{2} \eta \frac{d}{d\eta} (\chi^3) = \frac{d}{d\eta} \left(\chi^3 \frac{d\chi}{d\eta} \right), \quad (4.2)$$

with boundary conditions $\chi(\eta_0) = 0$ and $\chi \rightarrow 1$ as $\eta \rightarrow -\infty$. To solve this system numerically, we shoot from $\chi = 0$ and iterate to determine η_0 . The shooting requires a second boundary at $\eta = \eta_0$, which we determine in the regime $\chi \ll 1$ as

$$\chi = \frac{\eta_0}{2} (\eta_0 - \eta) + \dots \quad (4.3)$$

We find $\eta_0 \approx 1.578$. In figure 3*a*, we show that cross-sections of the numerical results become self-similar in the far-field. The similarity solution, $\chi(\eta)$, shows good agreement with the

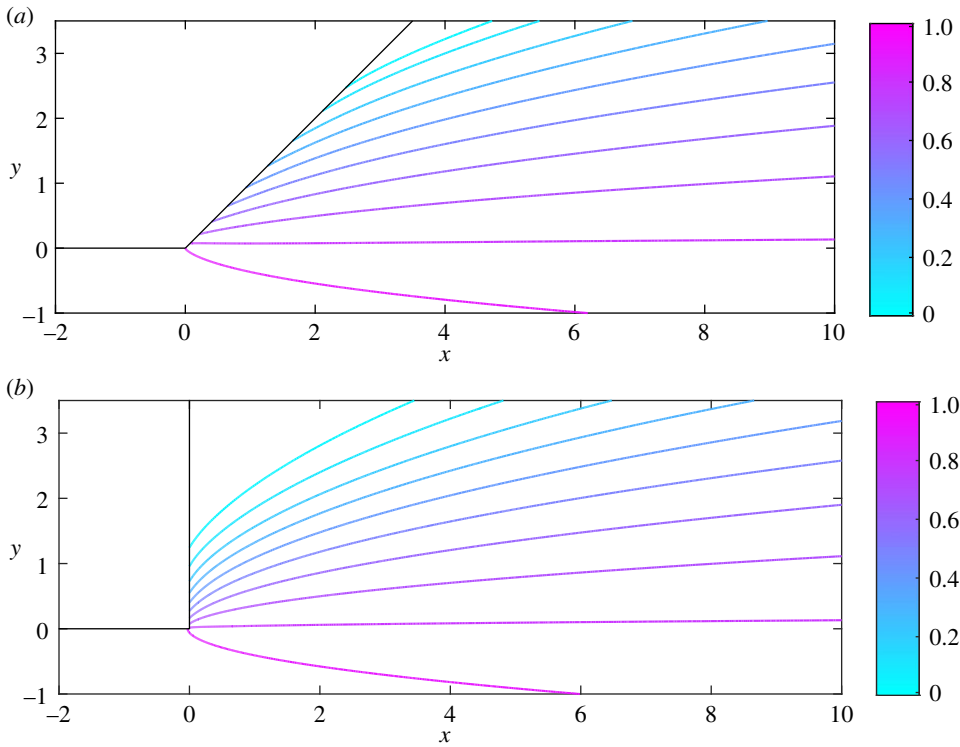


Figure 2. Contour plots of the dimensionless thickness of the steady flow, $h(x, y)$ in a channel that expands at $x = 0$ for two values of the opening angle, α : (a) $\alpha = \pi/4$ and (b) $\alpha = \pi/2$. The results are obtained numerically, as described in §3. Contours are plotted at $h = 0.01, 0.1, 0.2, 0.3, 0.4, 0.5, 0.6, 0.7, 0.8, 0.9$. (Online version in colour.)

numerical results for $x \gg 1$ as expected. For smaller x , the results diverge because the similarity solution neglects the influence of the angled wall and the downslope diffusive term, $\partial^2 h^4 / \partial x^2$ on the right-hand side of (2.3), both of which are important in $x \sim 1$. The flow depth along the line $y = 0^-$ is plotted for four values of the opening angle in figure 3b. The x gradients are relatively large near the wall vertex at $x = 0$ but quickly become negligible further downstream, as expected. The upstream flow depth is unity and the downstream flow depth is also constant, because along the line $y = 0$, the similarity variable is $\eta = 0$ and the flow depth is $\chi(0) = 0.812$.

5. Exact solution for $\alpha = \pi$

In the special case that the wall opening angle is $\alpha = \pi$, an exact solution for the flow depth can be obtained. We introduce the following conformal mapping of the physical space

$$s + it = 2(x + iy)^{1/2} \quad (5.1)$$

and in this case the domain now corresponds to $s > 0$. The governing equation (2.3) for the flow depth is recast as

$$\left(s \frac{\partial}{\partial s} - t \frac{\partial}{\partial t} \right) (h^3) = \left(\frac{\partial^2}{\partial s^2} + \frac{\partial^2}{\partial t^2} \right) \left(h^4 / 2 \right). \quad (5.2)$$

The far field conditions can be written as $h \rightarrow 1$ as $s \rightarrow -\infty$ and $h \rightarrow 0$ as $s \rightarrow +\infty$. The no-flux boundary condition on both sides of the wall ($y = 0^+$ and $y = 0^-$) is $\partial h / \partial y = 0$, which becomes

$$\frac{\partial h}{\partial s} = 0 \quad \text{on } s = 0. \quad (5.3)$$

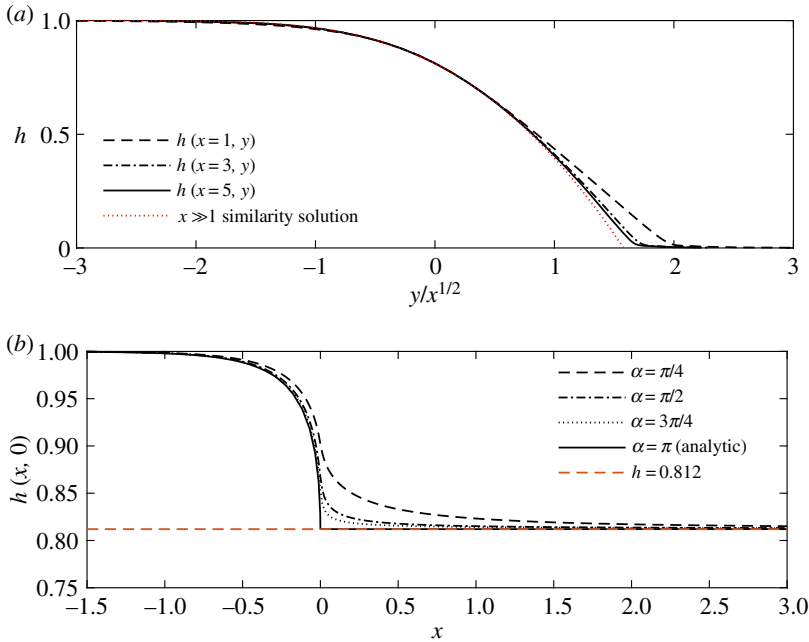


Figure 3. (a) Steady flow depth along three cross-sections ($x = 1, 3, 5$) in the case of a channel opening angle of $\alpha = \pi/2$ as a function of the similarity variable, $y/x^{1/2}$. The similarity solution (obtained in §4) provides good agreement with the numerical result for $x \geq 5$ for this value of α . There is slight divergence for very small h because the extra source term added for the numerical method has an influence here. (b) Steady flow depth along the line $y = 0^-$ as a function of streamwise distance for four values of the opening angle, α . The upstream flow depth is unity. The downstream flow depth is given by the similarity solution, which is a constant, $h(x, 0) = \chi(\eta = 0) = 0.812$. The numerically computed solutions adjust to the similarity value over relatively short lengths. The results are obtained through numerical integration of the governing partial differential equation (2.3), with the exception of the case $\alpha = \pi$, for which there is an analytic solution (see §5). (Online version in colour.)

This boundary condition suggests a solution of the form $h = \mathcal{H}(t)$ and upon substituting into (5.2), we find that $\mathcal{H}(t)$ satisfies the same ODE (4.2) and boundary conditions as $\chi(\eta)$. The complete solution is therefore given by

$$h = \chi \left\{ \pm \sqrt{2}[(x^2 + y^2)^{1/2} - x]^{1/2} \right\}, \quad (5.4)$$

where the argument of χ has positive sign when $y > 0$ and negative when $y < 0$. Contours of the height field (5.4) correspond to

$$y = \eta_* \left(x + \eta_*^2/4 \right)^{1/2}, \quad (5.5)$$

where $\chi(\eta_*) = h_*$. In particular the contact line $y_c(x)$ is given by $\eta_* = \eta_0$ (see §4). We plot the contours (5.5) for $h_* = 0.01, 0.4, 0.7$ in figure 4, showing excellent agreement with the numerically computed solution. We also note that when $x \gg 1$,

$$h = \chi \left(y/x^{1/2} \right) + \mathcal{O}(1/x), \quad (5.6)$$

thus recovering the downstream similarity solution (§4) and confirming that near-field corrections to it are $\mathcal{O}(1/x)$.

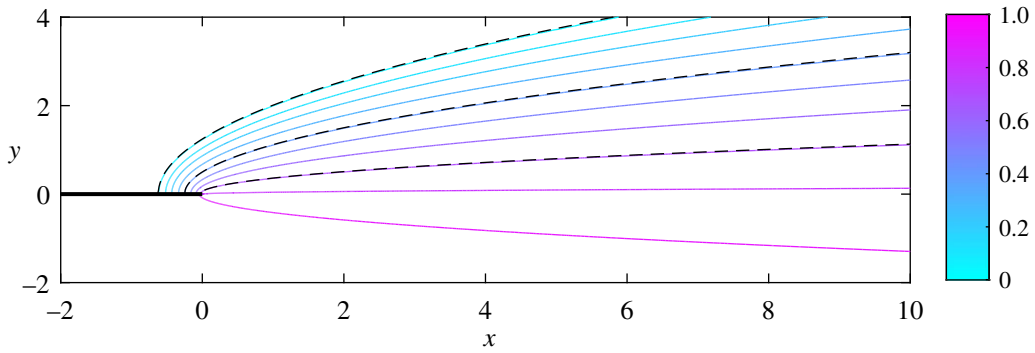


Figure 4. Contours of the steady flow depth for the case $\alpha = \pi$. Contours of the numerical result (continuous coloured lines) are plotted at $h = 0.01, 0.1, 0.2, 0.3, 0.4, 0.5, 0.6, 0.7, 0.8, 0.9$. The thick black line represents the wall. Contours of the exact solution (5.4), plotted as dashed lines for $h = 0.01, h = 0.4$ and $h = 0.7$ show excellent agreement. (Online version in colour.)

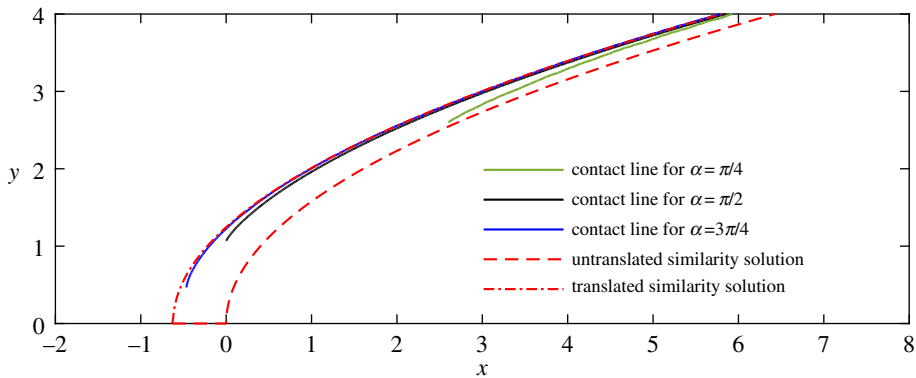


Figure 5. The position of the contact line as a function of downstream distance, x , obtained from our numerical method for three values of α . The translated similarity solution (which is also the exact solution for $\alpha = \pi$) provides a much better prediction for the contact line than the untranslated similarity solution. The agreement is good for all α but better for wider opening angles. (Online version in colour.)

6. The translated similarity solution

We can improve the agreement between the earlier similarity solution and the numerical computations for all α by translating it a distance $x = -x_1 < 0$ upstream. We use the similarity variable $\eta = y/(x + x_1)^{1/2}$ [19]. The idea is that this virtual origin accounts for the adjustment to the similarity solution in the region in which $x \sim 1$. The solution $\chi(\eta)$ is unchanged but is translated upstream a distance x_1 . The parameter x_1 is chosen to agree with the contact line from the exact solution for $\alpha = \pi$ (5.4); we use $x_1 = \eta_0^2/4 \approx 0.623$. We first note that the translated similarity solution does not agree precisely with the exact solution for $\alpha = \pi$ away from the contact line because the contours take the form given by (5.5). Of course, the solution converges to the similarity shape for large x , as before.

The prediction for the contact line from the translated similarity solution is significantly improved from the untranslated similarity solution even for $\alpha \neq \pi$ (figure 5). The agreement for the contact line between the similarity solution and the numerical results could be improved further still by allowing the location of the virtual origin to depend on α . However, the single choice of $x_1 = \eta_0^2/4$ provides sufficient agreement and enables the contact line to be simply approximated for any α .

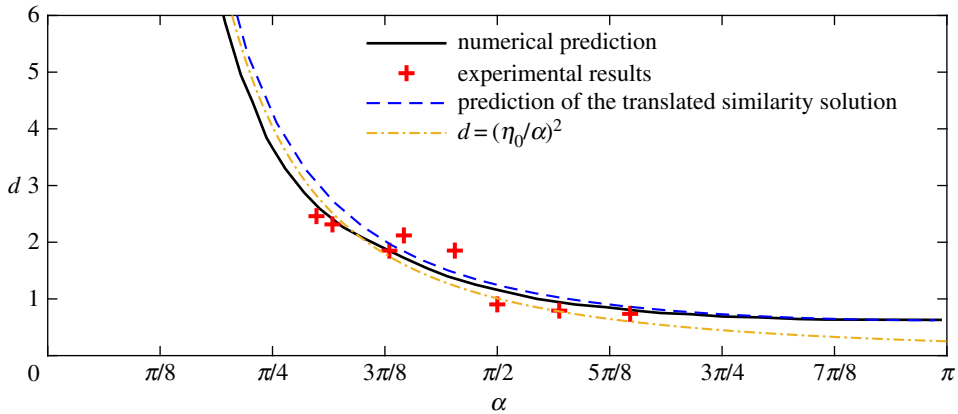


Figure 6. The distance along the wall, d , at which detachment occurs as a function of the channel opening angle, α . The prediction from our numerical simulations is plotted as a continuous black line and the red pluses indicate the experimental results (table 1). The prediction from the similarity solution (equation (6.2)) is plotted as a blue dashed line and we also include its behaviour as $\alpha \rightarrow 0$, which is $d = (\eta_0/\alpha)^2$ (a yellow dot-dashed line). (Online version in colour.)

Our prediction for the location of the contact line can be used to estimate the location of the detachment from the wall as a function of α . The similarity solution with virtual origin at $-x_1 = -\eta_0^2/4$ predicts that the shape of the current edge where $h = 0$ is given by

$$y = \eta_0(x + x_1)^{1/2}. \quad (6.1)$$

The intersection of the contact line (6.1) obtained from the similarity solution with the wall, $y = x \tan \alpha$, yields the following location for the detachment distance along the wall,

$$d = \frac{\eta_0^2}{2(1 - \cos \alpha)}. \quad (6.2)$$

This prediction is compared with the numerical results in figure 6. We note that locating the virtual origin at $-x_1 = -\eta_0^2/4$ provides good agreement for all angles of expansion and the agreement is exact at $\alpha = \pi$. As $\alpha \rightarrow 0$, equation (6.2) predicts that $d \sim (\eta_0/\alpha)^2$ and we include this in figure 6. It provides good agreement over the whole range of opening angles, α .

7. Laboratory experiments

We conducted a series of experiments in which golden syrup was released from a line source at constant flux onto a Perspex tank inclined at an angle $\beta = 10^\circ$. The line source was restricted to one side of the tank, which was bounded by a wall parallel to the direction of steepest descent down the slope. Further downstream, the wall opened at its vertex with angle α , which was varied. The region around the wall was cleaned each time the angle was changed to ensure that the influence of surface tension at the detachment point was consistent across all experiments. The syrup was released from a lock gate behind which the depth was maintained fixed by hand to ensure constant flux. When the steady state was attained, the flow depth upstream, H_∞ , was obtained by projecting a narrow laser line onto the free-surface and recording the difference between the deflection of the line in the absence of fluid [12,20]. In order for this method to be effective the fluid must be relatively opaque and this required the addition of a few drops of paint to the syrup. It was confirmed (through rheometer measurements) that the syrup remained Newtonian with dynamic viscosity 89.6 Pa s.

Table 1. Experimental results.

angle of opening α (degrees)	flow thickness H_∞ (mm)	wall distance D (mm)	wall distance d (dimensionless)
53.8	7.9	110	2.46
57.0	8.0	105	2.31
68.4	8.0	84	1.85
71.3	7.9	95	2.12
81.5	7.9	83	1.85
90.0	8.0	41	0.90
102.4	8.0	36	0.79
116.6	7.9	33	0.74

The dimensional detachment distance along the wall, D , was measured from photographic images of the steady flow and the results are shown in table 1. They show good agreement with the numerical predictions and analytical estimates from our theory (figure 6).

8. Discussion and conclusion

This contribution has described the spreading of viscous fluid into an expanding channel using the equations of Stokes flow and the lubrication approximation. The governing equation has been solved numerically and far downstream the shape of the flow depth is self-similar, being governed by a balance between the gravity-driven flux down the slope and the cross-slope gradients in the hydrostatic pressure. We have obtained an exact analytical solution to the complete system in the case that there is a single, semi-infinite wall ($\alpha = \pi$). This solution motivates translating the similarity solution, which provides very good predictions for the location of the contact line and the wall detachment distance as a function of the vertex angle. These results also show good agreement with our laboratory experiments.

Our investigation was motivated by the need to optimize the design of lava flow barriers, which are used to protect towns and infrastructure in many regions of volcanic hazard. The flow around a vertex studied here is analogous to the flow at the downstream side of a deflecting barrier, albeit that our flows are uniform upstream. Civil defence authorities are particularly interested in the size and shape of the downstream dry region and our results demonstrate that surprisingly this may be insensitive to the shape of the trailing side of the barrier (the contact line is always well-approximated by equation (6.1)). This suggests that the size of the dry zone is primarily controlled by the cross-stream width of the barrier and the upstream deflection of the oncoming flow. Therefore, efforts should be directed at ensuring the barrier is as wide as possible in the cross-stream direction and shaped to minimize the upstream flow depth and potential for overtopping, a problem that was analysed in [12]. It would be interesting to extend the present analysis to downstream boundaries with curved shape and explore whether the current thickness is also insensitive to the shape in this case.

Data accessibility. This article has no additional data.

Authors' contributions. A.J.H. and H.E.H. conceived the project. E.M.H. and A.J.H. carried out the experiments. E.M.H. drafted the manuscript. All authors read, suggested changes and approved the manuscript.

Competing interests. The authors declare that they have no competing interests.

Funding. E.M.H. is grateful for an EPSRC I-Case studentship funding his research (ref EP/P510440/1). This project was initiated at the 2018 Woods Hole Oceanographic Institution's Geophysical Fluid Dynamics programme, which is supported by the National Science Foundation (award number 1332750).

Acknowledgements. The authors gratefully acknowledge C. Gladstone, A. Pluck and A. W. Woods for their assistance and advice with the laboratory experiments. They also acknowledge many interesting and

References

1. Huppert HE. 2006 Gravity currents: a personal perspective. *J. Fluid Mech.* **554**, 299–322. (doi:10.1017/S002211200600930X)
2. Baxter SJ, Power H, Cliffe KA, Hibberd S. 2009 Three-dimensional thin film flow over and around an obstacle on an inclined plane. *Phys. Fluids* **21**, 032102. (doi:10.1063/1.3082218)
3. Dietterich HR, Cashman KV, Rust AC, Lev E. 2015 Diverting lava flows in the lab. *Nat. Geosci.* **8**, 494–496. (doi:10.1038/ngeo2470)
4. Stillwagon LE, Larson RG. 1988 Fundamentals of topographic substrate leveling. *J. Appl. Phys.* **63**, 5251–5258. (doi:10.1063/1.340388)
5. Kalliadasis S, Bielarz C, Homsy G. 2000 Steady free-surface thin film flows over topography. *Phys. Fluids* **12**, 1889–1898. (doi:10.1063/1.870438)
6. Mazouchi A, Homsy G. 2001 Free surface Stokes flow over topography. *Phys. Fluids* **13**, 2751–2761. (doi:10.1063/1.1401812)
7. Gaskell P, Jimack P, Sellier M, Thompson H, Wilson M. 2004 Gravity-driven flow of continuous thin liquid films on non-porous substrates with topography. *J. Fluid Mech.* **509**, 253–280. (doi:10.1017/S0022112004009425)
8. Aksel N, Schörner M. 2018 Films over topography: from creeping flow to linear stability, theory, and experiments, a review. *Acta Mech.* **229**, 1453–1482. (doi:10.1007/s00707-018-2146-y)
9. Hinton EM, Hogg AJ, Huppert HE. 2019 Interaction of viscous free-surface flows with topography. *J. Fluid Mech.* **876**, 912–938. (doi:10.1017/jfm.2019.588)
10. Sellier M, Lee Y, Thompson H, Gaskell P. 2009 Thin film flow on surfaces containing arbitrary occlusions. *Comput. Fluids* **38**, 171–182. (doi:10.1016/j.compfluid.2008.01.008)
11. Sellier M. 2015 Modelling the wetting of a solid occlusion by a liquid film. *Int. J. Multiph. Flow* **71**, 66–73. (doi:10.1016/j.ijmultiphaseflow.2014.12.007)
12. Hinton EM, Hogg AJ, Huppert HE. Submitted. Viscous free-surface flows past cylinders. *Phys. Rev. Fluids*.
13. Nusselt W. 1916 Die Oberflächenkondensation des Wasserdampfes. *VDI-Zs* **60**, 541.
14. Lister JR. 1992 Viscous flows down an inclined plane from point and line sources. *J. Fluid Mech.* **242**, 631–653. (doi:10.1017/S0022112092002520)
15. Batchelor GK. 1965 *An introduction to fluid dynamics*. Cambridge, UK: Cambridge University Press.
16. Vellingiri R, Savva N, Kalliadasis S. 2011 Droplet spreading on chemically heterogeneous substrates. *Phys. Rev. E Stat. Nonlin. Soft Matter Phys.* **84**, 1–14. (doi:10.1103/PhysRevE.84.036305)
17. Thompson BW. 1968 Secondary flow in a Hele-Shaw cell. *J. Fluid Mech.* **31**, 379–395. (doi:10.1017/S0022112068000212)
18. Smith PC. 1973 A similarity solution for slow viscous flow down an inclined plane. *J. Fluid Mech.* **58**, 275–288. (doi:10.1017/S0022112073002594)
19. Barenblatt GI, Isaakovich BG. 1996 *Scaling, self-similarity, and intermediate asymptotics: dimensional analysis and intermediate asymptotics*, vol. 14. Cambridge, UK: Cambridge University Press.
20. Hewitt DR, Balmforth NJ. 2013 Thixotropic gravity currents. *J. Fluid Mech.* **727**, 56–82. (doi:10.1017/jfm.2013.235)